

T H E S I S

BOILER TEST AT SOUTHERN RAILWAY POWER HOUSE.

For the Degree of

BACHELOR OF SCIENCE

in

MECHANICAL ENGINEERING

by

J. C. MAYES.

Under

Prof. J. A. Switzer.

The plant of the Southern Railway Shops, at Knoxville, Tennessee, was tested on March 31st, and April 1st, 1909 by B. L. Thomas, Bruce Helm and J. C. Mayes, with the aid of the Junior and Senior engineers.

B. L. Thomas was in charge of the turbine test, Bruce Helm had charge of the air compressor test and J.C. Mayes was in charge of the boiler and furnace test.

The plant consists of battery of four 300 H.P. Sterling boilers fed with Roney stokers, run by an 8 H.P. Edison engine, an Ingersoll-Rand, two-stage compressor with twin engines, a Cochrane open feed-water heater, one 750 K.W. and one 350 K.W. Parsons steam turbine, with a 25 and $17\frac{1}{2}$ K.W. exciter respectively.

Commencing with the boilers, I will say that they were in fairly good condition. They all were cleaned out between four and six weeks of the time the test was made. The feed-water was good being clear and containing very little solid matter.

The shell of the boilers was completely covered over the top by a double layer of brick and cement, which serves as a good non-conductor of heat.

The steam line from each boiler was covered with asbestos and immediately led into one main line from which it was carried to the various departments of the plant by means of smaller pipes.

In the operation of the plant the water that fed the boiler was taken from the city supply, passed through the open heater,

and raised to the temperature of about 180° F by the exhaust steam which came from the compressor and turbines. From the heater it was taken into a hot water pump by means of gravity and fed into the different boilers.

The coal used by the plant is dumped on the outside of the boiler room and passed through a crusher, and by means of a conveyor is carried to the top of the boiler room and automatically dumped into bins over each boiler and then carried by means of chutes to small hoppers in front of each boiler and the coal's own weight fed itself onto the rocking grates.

When we started the test we put a blind flange into the exhaust line from the compressor and turbines and turned the exhaust into a feed-water heater not now in use by the plant and used the condensing water which was taken from the city main as feed-water for the boilers.

The feed-water was weighed by means of three raised tanks, each emptying into a larger tank and from there flowed by means of gravity into a hot water pump and then forced into the boilers. The temperature of the feed-water was taken in the large tank, but it was found that a correction of 2° had to be made owing to the fact that the water had to pass through 90 feet of piping before reaching the pump. Corrected readings only are recorded on the log sheet.

The boiler test was made as prescribed by the A.S.M.E. and all precautions were taken to make it reliable.

The coal for this test was weighed by the car load and par-

ticular care was taken to have all the unweighed coal out of the bin when the test was started.

In order to do this the boilers were fired by hand from coal placed on the floor until the test began. Owing to the intense heat of the furnace the grate bars had to be kept wet and this prevented us from getting the temperature of the ashes. The ashes were dropped down into a bin in the basement of the boiler room and from there were carried by the same conveyor that handled the coal into an ash bin and there allowed to accumulate during the entire test. They were then emptied into a car and weighed. Several samples were taken while they were emptying into the car and brought to the University and weighed and dried to determine the amount of moisture in order to find the actual amount of ash produced during the test.

The test lasted for 23 hours and 38 minutes, beginning at 9 A.M. March 31st and ending 8:38 A.M. April 1st, 1909.

Readings were taken at 15 minute intervals except in some cases where the state of things seem to remain constant.

As I have already stated the temperature of feed-water was taken from the large receiving tank. The temperature of the flue gas was taken just outside the boiler room, before entering the chimney by means of a pyrometer, the draught measured by a U tube manometer, and flue gas analysis made at frequent intervals. The temperature of the boiler room, also of external air was also taken. The calorimeter test of the steam was taken in the power house on account of there being no place to attach the calorimeter

in the boiler room.

A string was placed around each glass tube at the level of the water, in the beginning of the test and it was found that water stood approximately 8 inches in the tubes and this was taken as the initial point, reading above being recorded as plus and below minus. The average reading of the four water gauges, also of the four pressure gauges only are recorded on the log sheet. The temperature of the steam was found from steam tables.

A small amount of coal was taken from the hopper in front of each boiler every half hour, then at the end of every five hours this amount was quartered down to a quart and afterwards brought to the University and by means of the Parr calorimeter the B.T.U.'s per pound of coal determined, also the percent of surface and total moisture.

There was a small steady leakage from the blow-off of one of the boilers and the amount lost during the test was calculated by finding the amount lost in a given time. The total amount lost was found to be 2000 pounds. This is to be taken from the total amount of water pumped into the boilers.

Mechanical Laboratory—UNIVERSITY OF TENNESSEE

LOG OF BOILER TEST

Made by J. C. MayesDate March, 31, 1909Kind of Boiler StirlingMfg. by B & W

No.	TIME	PRESSURES			TEMPERATURES							WATER GAUGE	
		BAROMETER	STEAM GAUGE	DRAFT GAUGE	EXTERNAL AIR	BOILER ROOM	FLUE	FEED-WATER	CALORIMETER	STEAM	FURNACE	FROM INITIAL	Calori meter "Hg"
1	9.00 ^{AM}	29.11	142	1.000	56	79	730	145		330		0.000	
2	9.30		124	.875	54	79	715	149		323		4.75	
3	10.00	29.13	135	.875	54	80	710	156		330		-2.50	
4	10.30		119	.820	54	81	700	159		321		7.50	
5	10.45		113	.875	55	80	710	165		317		8.25	
6	11.00	29.12	111	.875	55	80	700	167		315		4.50	
7	11.15		116	.820	55	80	700	162		318		-2.00	
8	11.30		118	.820	54	81	700	147		320		-1.25	0.9
9	11.45 ^{PM}		113	.875	54	81	700	157		317		13.00	
10	12.00	29.11	114	.875	55	82	700	168	270	318		13.75	1.1
11	12.15		140	.820	56	81	690	178		332		6.00	
12	12.30		147	.750	55	82	660	178	278	336		9.75	1.4
13	12.45		141	.820	56	81	680	170	276	332		8.25	
14	1.00	29.10	143	.820	57	84	680	141	276	333		15.25	0.7
15	1.15		135	.820	56	84	690	141		330		12.00	
16	1.30		139	.750	57	84	680	152	274	332		9.00	1.5
17	1.45		140	.875	57	84	680	168		332		-0.50	
18	2.00	29.07	135	.875	59	84	700	159	276	330		5.00	1.6
19	2.15		144	.875	57	84	680	158		334			
20	2.30		145	.820	58	84	700	151	268	335		14.25	1.6
21	2.45		140	.875	58	83	680	157		332			
22	3.00	29.06	144	.820	58	84	670	161	265	334		5.00	1.6
23	3.15		134	.820	58	85	680	168		329			
24	3.30		137	.875	58	85	680	146	266	331		13.50	1.6
25	3.45		144	.875	57	85	690	157		334			
26	4.00	29.05	136	.875	57	85	690	145	266	330		14.75	1.6
27	4.15		135	.820	57	85	670	151		330			
28	4.30		138	.875	57	84	660	169	274	331		0.25	1.6
29	4.45		135	.820	57	83	630	110		330			
30	5.00	29.05	136	.820	56	84	660	120	275	330		15.25	1.8
31	5.15		131	.820	56	84	640	137		328			
32	5.30		140	.820	52	83	690	170	280	332		10.50	1.8
33	5.45		148	.820	53	85	650	176		337			
34	6.00	29.06	143	.820	53	86	650	175	278	334		11.00	1.8
35	6.15		139	.820	52	85	660	173	273	332			1.8

Mechanical Laboratory—UNIVERSITY OF TENNESSEE

LOG OF BOILER TEST

Made by..... Date.....

Kind of Boiler..... Mfg. by.....

No.	TIME	PRESSURES			TEMPERATURES							WATER GAUGE	
		BAROMETER	STEAM GAUGE	DRAFT GAUGE	EXTERNAL AIR	BOILER ROOM	FLUE	FEED-WATER	CALORIMETER	STEAM	FURNACE	FROM INITIAL	CALORIMETER MAXIMUM EXCESS
1	6.30		147	820	52	84	630	161	278	335		6.50	1.8
2	6.45		140	820	51	84	620	149		332			
3	7.00	29.07	142	820	50	83	610	144	278	333		6.50	1.8
4	7.15		142	820	49	83	640	141		333			
5	7.30		143	820	49	82	640	156	278	333		6.50	1.8
6	7.45		139	820	49	82	664	156		332			
7	8.00	29.08	142	1000	48	79	680	147	275	333		-1.25	1.8
8	8.15		142	935	48	80	670	134		333			
9	8.30		139	935	47	81	645	134	277	332		7.75	1.8
10	8.45		145	875	47	80	643	133		334			
11	9.00	29.09	140	825	47	82	660	128	277	332		4.75	1.8
12	9.15		141	1250	46	84	660	138		332			
13	9.30		143	875	46	84	655	148	277	334		6.50	1.4
14	9.45		143	935	45	88	655	142		337			
15	10.00	29.10	140	875	45	90	660	143	277	332		4.75	
16	10.15		150	875	45	86	670	156		332			
17	10.30		141	935	44	83	665	156		330		5.50	
18	10.45		141	935	44	82	670	153		327			
19	11.00	29.10	136	875	44	84	685	139		332		6.00	
20	11.15		131	875	43	81	682	146		334			
21	11.30		141	875	43	81	685	149		334		8.75	
22	11.45		142	875	42	79	670	149		335			
23	12.00	29.11	144	875	42	79	680	142		333		8.50	
24	12.15		142	820	42	79	655	145		336			
25	12.30		148	875	40	79	655	155		330		4.25	
26	12.45		136	935	41	81	680	158		330			
27	1.00	29.12	136	875	39	81	650	158		329		7.50	
28	1.15		134	875	40	80	680	150		332			
29	1.30		139	875	39	81	685	144		334		7.50	
30	1.45		143	875	40	80	670	138		336			
31	2.00	29.11	148	1000	40	82	690	148		330		2.75	
32	2.15		136	935	40	81	695	152		334			
33	2.30		145	935	40	82	700	148		330		4.50	
34	2.45		139	935	40	81	670	156		334			
35	3.00	29.10	137	875	39	80	640	140		331		8.00	

Mechanical Laboratory—UNIVERSITY OF TENNESSEE

LOG OF BOILER TEST

Made by..... Date.....

Kind of Boiler..... Mfg. by.....

No.	TIME	PRESSURES			TEMPERATURES							WATER GAUGE
		BAROMETER	STEAM GAUGE	DRAFT GAUGE	EXTERNAL AIR	BOILER ROOM	FLUE	FEED-WATER	CALORIMETER	STEAM	FURNACE	
1	3.15		139	935	38	81	650	136		332		6.00
2	3.30		146	935	39	81	660	132		335		
3	3.45		145	875	39	80	665	133		335		3.00
4	4.00	29.11	141	875	39	82	650	134		333		
5	4.15		142	875	39	76	675	144		333		5.00
6	4.30		146	875	39	74	695	144		335		
7	4.45		149	1000	39	75	670	144		337		7.00
8	5.00	29.12	144	935	40	79	630	134		334		
9	5.15		141	875	40	78	630	128		333		6.00
10	5.30		141	875	40	80	630	130		333		
11	5.45		136	875	40	80	600	124		330		2.75
12	6.00	29.12	133	875	40	79	630	109		328		
13	6.15		124	875	41	75	642	123		324		-1.25
14	6.30		129	935	41	75	690	117		326		
15	6.45		121	875	41	76	705	118		321		5.50
16	7.00	29.10	139	1000	41	76	705	103		332		
17	7.15		140	1000	42	76	720	109		332		0.50
18	7.30				42	75	660	127				
19	7.45				42	75						
20	8.00	29.05	139		42	77				332		
21	8.15				46	75	720	168				2.00
22	8.30				47	76						
23	8.38		128	897	48	78	735	168		326		6.00
24												
25												
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29												
30												
31												
32												
33												
34												
35	ave.	29.09	137	871	46	80	673	149	274	330		

Mechanical Laboratory—UNIVERSITY OF TENNESSEE

REPORT OF BOILER TEST

Made by *J. C. Mayes*Date *March 31, 1909.*Kind of Boiler *Stirling, Battery of Four* Manufactured by *B & W.*

Duration of trial	Hours.	<i>23.5</i>	FLUE GAS.		<i>B.W.-B</i>
DIMENSIONS. of Each			CO ₂	Per cent. of volume	<i>6.2-4.2</i>
Grate surface: length <i>7 3/4</i> ft., width <i>10</i> ft.	Sq. ft.	<i>73.4</i>	CO	" " "	<i>0 0</i>
Water heating surface	"	<i>3028</i>	H	" " "	<i>13.6-14.5</i>
Superheating surface	"		Free oxygen	" " "	
Height, chimney	Ft.	<i>125</i>	Air	Excess co-efficient,	
Ratio of draught area to grate			Quality of steam	Per cent.	<i>98.6</i>
Area, chimney	Sq. ft.	<i>26.7</i>	Superheat	Degrees,	<i>0</i>
Tubes: Diameter	No.	<i>3 1/2</i>	TOTAL WATER.		
Ratio heating to grate surface		<i>41</i>	Total weight water used	Pounds,	<i>729437</i>
PRESSURE.			Total evaporated, dry steam	"	<i>719226</i>
Barometer	Inches mercury	<i>29.09</i>	Factor of evaporation		<i>1.11</i>
Steam gauge	Pounds	<i>137</i>	Equivalent evaporated from and at 212°	"	<i>798337</i>
Absolute steam pressure	Pounds	<i>151.2</i>	WATER—PER HOUR.		
Draught gauge, near damper	Inches water	<i>0.871</i>	Amount used	Pounds,	<i>31080</i>
" " in ash pit	" "		Evaporated dry steam	"	<i>30603</i>
TEMPERATURE.			Equivalent evaporated from and at 212°	"	<i>33969</i>
External air	Degrees F.	<i>46</i>	ECONOMIC EVAPORATION.		
Boiler room	"	<i>80</i>	Per Pound of Fuel.		
Escaping gases	"	<i>673</i>	Actual, per lb. dry coal	Pounds,	<i>5.3</i>
Furnace	"		Equivalent from and at 212° [dry coal]	"	<i>6.2</i>
Feed water	"	<i>149</i>	Per Pound of Combustible		
Steam	"	<i>330</i>	Actual	Pounds	<i>6.8</i>
FUEL.			Equivalent evaporated from and at 212°	"	<i>7.9</i>
Kind of coal	<i>Sagamore Slack</i>		RATE OF EVAPORATION.		
Locality	<i>Frymouth Ky.</i>		Per Sq. Foot of Grate per Hour		
Size of coal	<i>Crushed.</i>		Actual from feed-water temperature	Pounds	<i>104.2</i>
Fixed carbon	Per cent.		Equivalent from and at 212°	"	<i>115.7</i>
Volatile matter	"		Per sq. Foot of Water-heating Surface per Hour.		
Moisture	<i>surface</i>	<i>1.73</i>	Actual	Pounds	<i>2.6</i>
Ash	"	<i>39200</i>	Equivalent from and at 212°	"	<i>2.8</i>
B. T. U. per pound coal		<i>10771</i>	Per sq. Foot of Least Draught Area per Hour.		
" " combustible		<i>10370</i>	Actual	Pounds,	
Carbon in ash	Per cent.		Equivalent from and at 212°	"	
Total coal consumed	Pounds.	<i>137400</i>	HORSE POWER.		
Total wood	"		*On basis 34 1/2 pounds equiv. evap. per hour		
Moisture in coal <i>Total</i>	Per cent.	<i>1.88</i>	Builders' rating	H. P.	<i>984</i>
Dry coal consumed	Pounds.	<i>134817</i>	Ratio of commercial to builders' rating	%	<i>1200</i>
Total refuse, dry	"	<i>31086</i>			
Total refuse, dry	Per cent.	<i>23</i>	Heat generated per pound dry coal	B. T. U.	<i>10171</i>
(c) Total combustible	Pounds.	<i>103632</i>	Heat absorbed per pound dry coal	"	<i>17629</i>
COMBUSTION—PER HOUR.			Heat lost in flue per pound dry coal	"	
Dry coal		<i>5694</i>	" " incomplete combustion lb. of coal	"	
(c) Combustible		<i>4409</i>	" " in refuse, lb. of coal	"	
Dry coal per square foot of grate		<i>19.4</i>	" " by radiation, etc., lb. coal	"	
Combustible per " " "		<i>15.01</i>	(a) Efficiency of boiler	%	
Dry coal per " " heating surface		<i>2.13</i>	(b) Efficiency of boiler and grate	%	
Combustible per " " "		<i>2.75</i>			<i>56</i>

NOTE.—Actual evaporation signifies the evaporation from feed-water temperature to dry steam at gauge pressure. It is apparent evaporation corrected for calorimeter determination.

*Standard commercial H. P. (a) Computed from combustible. (b) Computed from coal.

(c) This is dry coal less refuse.

(3)

